

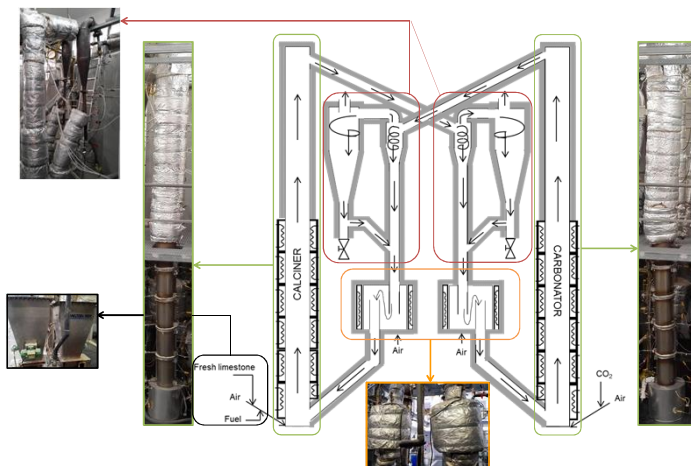
# Screening CO<sub>2</sub> capture test for cement plants using a lab scale Calcium Looping pilot facility.

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## Objective

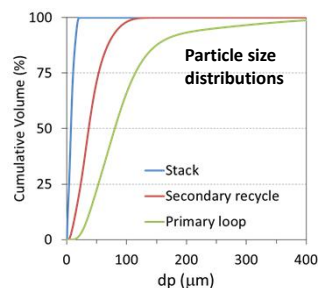
Calcium Looping (CaL) is based on the use of CaO as a regenerable sorbent of CO<sub>2</sub>. The technology has been demonstrated for post-combustion CO<sub>2</sub> capture in power generation at TRL 6-7, but requires detailed testing at closer conditions to those expected in cement applications: higher CO<sub>2</sub> concentrations, higher sorbent activity and lower average particle sizes. We investigate these new operating conditions in a 30 kW<sub>th</sub> CaL pilot in CEMCAP.

## THE 30 kW TEST FACILITY

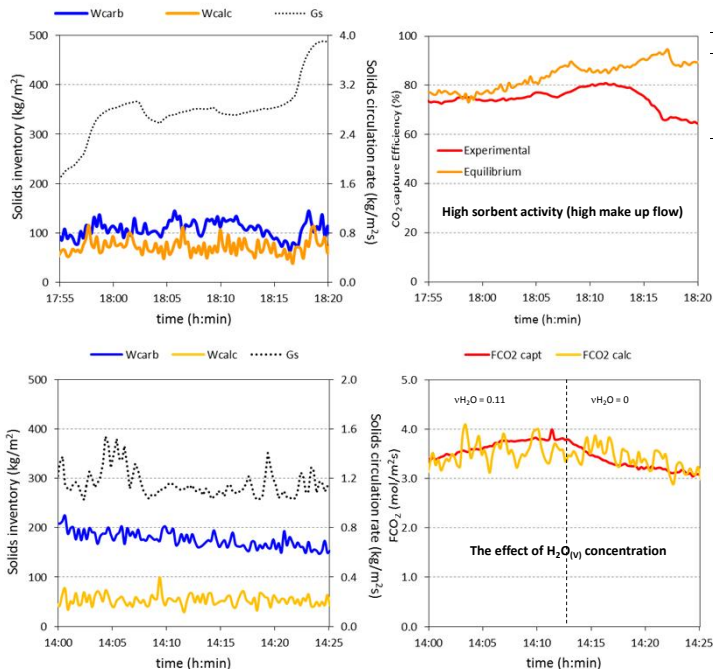


## MAIN FEATURES

- Two CFB reactors (h = 6 m, d<sub>i</sub> = 0.1 m)
- Double recycle loop
- Gas mixtures of CO<sub>2</sub>, air, SO<sub>2</sub>, H<sub>2</sub>O feeds
- 40 Thermocouples, 20 ΔP measurements
- 4 O<sub>2</sub> zirconia probes,
- 2 on-line gas analysers (CO<sub>2</sub>, O<sub>2</sub>, SO<sub>2</sub>, NO<sub>x</sub>)



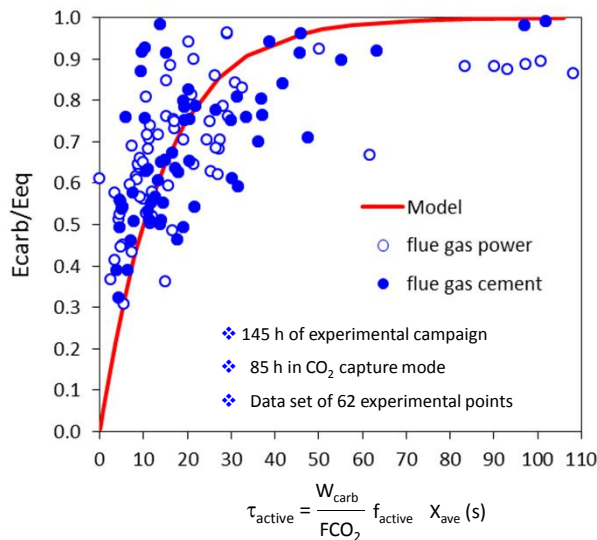
## EXAMPLES OF EXPERIMENTAL RESULTS OF CO<sub>2</sub> CAPTURE



## REACTION MASS BALANCE

### RANGE OF OPERATING CONDITIONS

| CARBONATOR                                     |                           | CALCINER  |                            |
|--|---------------------------|---|----------------------------|
| Carbonator temperature (°C)                    | T <sub>carb</sub> 620-725 | Calciner temperature (°C)                         | T <sub>calc</sub> 760-920  |
| Carbonator inlet velocity (m/s)                | U <sub>carb</sub> 2-3.7   | Calciner inlet velocity (m/s)                     | U <sub>calc</sub> 1.5-3.3  |
| Inlet CO <sub>2</sub> concentration (vol/vol)  | vCO <sub>2</sub> 0.1-0.27 | Molar ratio fresh make-up to CO <sub>2</sub>      | F0/FCO <sub>2</sub> 0-0.55 |
| Inlet H <sub>2</sub> O concentration (vol/vol) | vH <sub>2</sub> O 0-0.12  | Solids circulation flowrate (kg/m <sup>2</sup> s) | Gs 0.9-3.7                 |



## CONCLUSIONS

- High activity material resulting from large make up flows of limestone allow for high CO<sub>2</sub> capture efficiencies despite very low solids inventory in the reactor (100 kg/m<sup>2</sup>).
- Pilot plant and its reactor model behaves with similarly with flue gases from cement than with flue gases from power when using limestone as make up.

## References

- Hornberger M., Spörl R., Scheffknecht G., "Calcium Looping for CO<sub>2</sub> capture in cement plants – Pilot scale test". 13th Conference on Greenhouse Gas Control Technologies (GHGT-13), Lausanne, Switzerland.
- Spinelli M., Martínez I., De Lena E., Cinti G., Hornberger M., Spörl R., Abanades J.C., Mathai R., Fleiger K., Hoenig V., Gatti M., Campanari, S., Consonni S., Romano M.C. "Integration of Ca-Looping systems for CO<sub>2</sub> capture in cement plants". 13th Conference on Greenhouse Gas Control Technologies (GHGT-13), Lausanne, Switzerland.
- Charitos, A.; Rodríguez, N.; Hawthorne, C.; Alonso, M.; Zieba, M.; Arias, B.; Kopanakis, G.; Scheffknecht, G.; Abanades, J. C., "Experimental Validation of the Calcium Looping CO<sub>2</sub> Capture Process with Two Circulating Fluidized Bed Carbonator Reactors". *Ind. Eng. Chem. Res.* 2011, 50, 9685-95.
- Rodríguez, N.; Alonso, M.; Abanades, J. C., "Experimental Investigation of a Circulating Fluidized-Bed Reactor to Capture CO<sub>2</sub> with CaO". *AIChE J.*, 2011, 57, 1356-66.

$$\tau_{\text{active}} = \frac{W_{\text{carb}}}{\text{FCO}_2} f_{\text{active}} X_{\text{ave}} (\text{s})$$